



# Sulphuric acid and Pt treatment of the photocatalytically active titanium dioxide

D.V. Kozlov\*, A.V. Vorontsov

Boriskov Institute of Catalysis and Novosibirsk State University, Novosibirsk 630090, Russian Federation

## ARTICLE INFO

### Article history:

Received 31 March 2008

Revised 26 May 2008

Accepted 30 May 2008

Available online 30 June 2008

### Keywords:

Titanium dioxide

Gas phase photocatalytic oxidation

Surface acidity

Low temperature CO adsorption

Surface titration

## ABSTRACT

The study focuses on preparation, surface sites characterization and catalytic activity testing of pure ( $\text{TiO}_2$ ), sulfated ( $\text{TiO}_2\text{-S}$ ), loaded with 1 wt% Pt ( $\text{TiO}_2\text{-Pt}$ ) and platinumized/sulfated ( $\text{TiO}_2\text{-Pt-S}$ ) high surface area anatase  $\text{TiO}_2$  (100% anatase,  $340 \text{ m}^2/\text{g}$ ). Sulfation was performed in 4 M  $\text{H}_2\text{SO}_4$  solution and was not followed by a high temperature calcination. TEM images reveal the formation of a 3 Å amorphous layer over  $\text{TiO}_2$  and  $\text{TiO}_2\text{-Pt}$  surface after their sulfation. Infrared spectrum of  $\text{TiO}_2\text{-S}$  contains additional absorption bands at 1235, 1333 and  $1378 \text{ cm}^{-1}$  that are assigned to S=O stretch and distorted adsorbed  $\text{SO}_4^{2-}$  vibrations. Low temperature CO adsorption and organic species adsorption from heptane solutions was performed for characterization of surface sites.  $\text{TiO}_2\text{-S}$  showed 3–5  $\text{cm}^{-1}$  shift of adsorbed CO absorption band compared to initial  $\text{TiO}_2$ . The quantity of adsorbed CO increased by a factor of 1.5 for  $\text{TiO}_2\text{-S}$  indicating the increase of the quantity of surface Lewis sites. Sulfation also resulted in disappearance of OH groups having absorption band at  $3690 \text{ cm}^{-1}$  that was attributed to substitution by monodentate and bidentate sulfates. Four bases and two acids with different pK were used as probes in solution titration revealing that the quantity of different acid sites in  $\text{TiO}_2\text{-S}$  increases 1.07–2.17 times. Unexpectedly the quantity of acid and base sites in  $\text{TiO}_2\text{-Pt-S}$  decreases relatively to other catalysts studied.

Catalytic activity of the samples in acetone deep photooxidation was measured as a function of acetone vapor concentration in a flow-circulating reactor. All dependences are well described by the one site Langmuir–Hinshelwood kinetic model. The maximum oxidation rate was similar for all samples and was observed at acetone concentration above 1500 ppm. However, in the range of low acetone concentration the activity of  $\text{TiO}_2\text{-Pt-S}$  was about triple of pure  $\text{TiO}_2$  activity. The high activity of sulfated/platinumized and sulfated  $\text{TiO}_2$  is due to the much increased acetone adsorption constant.

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## 1. Introduction

The sulfation of titanium dioxide was recently acknowledged as a way of enhancing its catalytic and photocatalytic activity. Reputable companies like Sachtleben Chemie GmbH are producing titanium dioxide containing several percent of sulfur in the form of sulfates for catalytic applications. Two companies in Russia which are producing photocatalytic air cleaners already use only sulfated  $\text{TiO}_2$  because it demonstrates higher photocatalytic oxidation (PCO) rates for a variety of organic compounds. At the same time, the nature of PCO rates increase if any is still under active investigation and discussed by many researchers.

The evolution of understanding of the influence of  $\text{TiO}_2$  acidic properties on its (photo)catalytic activity started from the 80's of the last century when researchers [1,2] had demonstrated the role of the number of hydroxyl groups on the oxygen photoadsorption. Later Papp et al. [3] measured the number of  $\text{TiO}_2$  (Degussa

P25 annealed at different temperatures) surface hydroxyl groups by the *n*-butylamine titration method [4] and revealed the correlation between this number and the rate of 1,4-dichlorobenzene photocatalytic oxidation in water solution. Kwon et al. [5] obtained the similar result with the  $\text{WO}_3/\text{TiO}_2$  photocatalyst in the same reaction. Authors supposed that the increased surface acidity and therefore increased  $\text{TiO}_2$  adsorption affinity was the main factor responsible for the photocatalytic activity increase.

Kantoh and Okazaki [6] investigated  $\text{TiO}_2$  samples prepared from titanium tetraisopropoxide and  $\text{TiOSO}_4$ . The  $\text{TiO}_2$  sample prepared from  $\text{TiOSO}_4$  had both types of acid sites—Brønsted and Lewis, the later ones being converted into the Brønsted sites after addition of water due to the bidentate sulfate  $-\text{Ti}-\text{O}-\text{SO}_2-\text{O}-\text{Ti}-$  reaction. They also revealed the correlation between the amount of surface OH groups and the amount of reacting aminoalcohols in the autoclave.

Closely to the  $\text{TiO}_2$  sulfation treatment, Deng et al. [7] prepared several  $\text{TiO}_2$  samples using the sol–gel method and treated some of them with  $\text{H}_2\text{SO}_4$ . They demonstrated that the sulfated samples had a higher conversion and stability during the gas phase photocatalytic oxidation of hexane, benzene and methanol. The authors

\* Corresponding author.

E-mail address: kdvd@catalysis.ru (D.V. Kozlov).

explained such behavior by the two simultaneous trends: the increase of the surface area of sulfated samples and the increase of their surface acidity. The first reason was the main according to the authors.

Colon et al. [8] also demonstrated that sulfated TiO<sub>2</sub> annealed at 600–700 °C had a higher photocatalytic activity in the water phase phenol PCO than pure TiO<sub>2</sub>. The SO<sub>4</sub><sup>2-</sup> ions were almost absent after the high temperature treatment. The authors attributed this effect to the TiO<sub>2</sub> surface stabilization by sulfates during the annealing and keeping a higher specific surface area compared with the pure untreated TiO<sub>2</sub>. In their later work [9] the authors developed their previous conclusions and stated that the annealing of the sulfated samples leads to the creation of bulk oxygen vacancies through the dehydroxylation of the excess of adsorbed water giving a highly defective photocatalyst. It gives an enhancement of the PCO activity due to the improvement of the charge separation and diffusion to the surface. In their most recent work [10] these researchers conducted simultaneous TiO<sub>2</sub> sulfation and Pt deposition and demonstrated that the samples obtained are more active in the phenol PCO in water. The authors make the reasonable guess that the Pt deposition is affected by the preliminary sulfation giving the higher dispersion of obtained Pt particles. Other researchers [11] also attributed the improved activity of SO<sub>4</sub><sup>2-</sup>/TiO<sub>2</sub> to the surface area increase.

Keller et al. [12,13] observed higher time on stream stability of sulfated sol-gel TiO<sub>2</sub> in gaseous toluene photocatalytic oxidation. Higher concentrations of H<sub>2</sub>SO<sub>4</sub> resulted in higher photocatalytic activities. They attributed the enhanced stability to a lower adsorption of toluene over the catalyst surface and possible increased electron-hole pairs separation. Muggli and Ding [14], on the contrary, observed higher adsorption of gaseous organic compounds. They also registered increased catalytic stability of sulfated TiO<sub>2</sub> compared to unsulfated one. As in the previously mentioned works, these authors used high temperature calcination after the H<sub>2</sub>SO<sub>4</sub> treatment.

Yu with co-workers [15] suggested that the promoting effect of sulphuric acid is explained by the removal of sodium ion impurities from the glass used as a support during the TiO<sub>2</sub> thin films preparation.

Results which were cited above could not explain the enhanced photocatalytic activity of photocatalyst obtained by mild H<sub>2</sub>SO<sub>4</sub> treatment with consequent washing and drying at a low (less than 150 °C) temperature since such SO<sub>4</sub><sup>2-</sup>/TiO<sub>2</sub> samples contain much higher quantity of surface sulfates. In this case, the chemical and physico-chemical interactions of photocatalytic reaction substrates, products and intermediates should be taken into account. We had focused on such an approach in our previous research [16–18].

Platinum deposition has been used for a long time to enhance photocatalytic reactions over TiO<sub>2</sub> in liquid and gas phase [19–28]. Therefore, addition of Pt combined with sulfation is expected to provide further increase of TiO<sub>2</sub> photocatalytic activity. This opportunity was not investigated before for gas phase reactions. Moreover, platinum deposition over some kinds of TiO<sub>2</sub> can produce photocatalysts with decreased activity in gas phase reactions [29]. Of special interest is the capability of sulfuric acid treatment to improve the performance of these platinized TiO<sub>2</sub> samples.

In the present work, we employ the combination of platinum deposition and sulfation without subsequent high-temperature treatment in order to increase TiO<sub>2</sub> photocatalytic activity. The tandem of solution titration and CO adsorption methods is harnessed for characterization of TiO<sub>2</sub> surface acidity measurements, which is complemented by HR-TEM images of the catalyst surface.

Kinetic study on the acetone photocatalytic oxidation in a flow-circulating reactor reveals that sulfation of platinized TiO<sub>2</sub> results in strong increase of acetone adsorption constant that provides highly increased oxidation rate at the low acetone concentration

**Table 1**  
Specific surface area, Pt and S content for TiO<sub>2</sub>, TiO<sub>2</sub>-S and TiO<sub>2</sub>-Pt-S samples

Sample	S <sub>BET</sub> , m <sup>2</sup> /g	Pt content, wt%	S content, wt%
TiO <sub>2</sub>	341	–	–
TiO <sub>2</sub> -S	335	–	1.54
TiO <sub>2</sub> -Pt-S	–	0.95	1.45

while unmodified TiO<sub>2</sub> outperforms at the high acetone concentrations.

## 2. Experimental

### 2.1. Materials and catalyst preparation

Titanium dioxide Hombifine N (Sachtleben Chemie GmbH, 100% anatase, specific surface area 341 m<sup>2</sup>/g) was used as supplied. H<sub>2</sub>SO<sub>4</sub> (high-purity grade), H<sub>2</sub>PtCl<sub>6</sub>·6H<sub>2</sub>O (38.12 wt% Pt) were used for TiO<sub>2</sub> modification. Deionized water from a Barnsted EASYpure II ultrapure water system was used for solutions preparation and photocatalysts treatment.

The TiO<sub>2</sub> sulfation method was described previously [17] and was used here with a minor modification. A 1 g TiO<sub>2</sub> sample was placed into a round-bottomed 100 ml flask; 50 ml of the 4 M H<sub>2</sub>SO<sub>4</sub> aqueous solution was added. Then the flask was put into a thermostat and kept at 50 °C for 2 h under continuous stirring. Treated sample was then washed 6–7 times with deionized water with subsequent centrifugation. The amount of sulfates in the wash water was qualitatively controlled with a 1 M BaCl<sub>2</sub> solution. The prepared samples were finally dried in air at 120 °C for 2–3 h. Untreated initial TiO<sub>2</sub> sample and the sample modified with H<sub>2</sub>SO<sub>4</sub> are referred to further in the text as TiO<sub>2</sub> and TiO<sub>2</sub>-S, correspondingly.

To investigate the influence of Pt addition, a sample was prepared by the NaBH<sub>4</sub> reduction of adsorbed H<sub>2</sub>PtCl<sub>6</sub>. This sample is referred to as TiO<sub>2</sub>-Pt. Subsequent sulfation of this catalyst produced sample marked TiO<sub>2</sub>-Pt-S. Platinum deposition was performed according to the following method. 1 g of TiO<sub>2</sub> suspended in 20 ml of water was poured into a 50 ml beaker under stirring. Then 0.2 ml of 0.257 M H<sub>2</sub>PtCl<sub>6</sub> stabilized with 0.05 M HCl was added. The Pt reduction was conducted by the dropwise addition of the 3-fold molar excess of a cold NaBH<sub>4</sub> water solution. In our case it was 2 ml of 3 mg/ml NaBH<sub>4</sub> solution. The obtained precursor was washed 3 times with water and dried at 120 °C. The second step of preparation, sulfation, was identical to that for TiO<sub>2</sub>-S sample.

Specific surface area, platinum and sulfur content were measured by the low temperature nitrogen adsorption (ASAP 2400, USA) and by X-ray fluorescence analysis with VRA-20 instrument correspondingly. The results are summarized in Table 1.

Using the fact that Pt deposition does not influence the specific surface area [30] one can conclude from the data in Table 1 that it does not depend on the TiO<sub>2</sub> treatment in the present work and equals to about 340 m<sup>2</sup>/g for all the samples.

TEM images were obtained with a JEM-2010 transmission electron microscope to describe the TiO<sub>2</sub>, TiO<sub>2</sub>-S and TiO<sub>2</sub>-Pt-S samples.

### 2.2. Surface titration and CO adsorption methods

Surface titration method used in this work is based on the adsorption of organic acids and bases on the catalyst surface from anhydrous *n*-heptane (reference grade) solution [17]. Measurements of the probe species concentration in *n*-heptane solution were performed by a Perkin Elmer Lambda 35 UV/VIS spectrophotometer. The chemical formula, strength and spectroscopic data of the used probe species are presented in Table 2.

**Table 2**  
Thermodynamic and spectroscopic data on the probe species used in the surface titration experiments

Probe species	Strength, pK	$\lambda_{\max}$ , nm	Absorption coefficient $\varepsilon \times 10^{-3}$ , L/(mol cm)
<b>Acids</b>			
Benzoic acid, C <sub>7</sub> H <sub>6</sub> O <sub>2</sub>	pK <sub>a</sub> = 4.2	230	11.5
<i>o</i> -Nitrophenol, C <sub>6</sub> H <sub>4</sub> (NO <sub>2</sub> )(OH)	pK <sub>a</sub> = 7.17	270	6.81
<b>Bases</b>			
Piperidine, C <sub>5</sub> H <sub>11</sub> N	pK <sub>b</sub> = 2.88	211	0.975
Pyridine, C <sub>5</sub> H <sub>5</sub> N	pK <sub>b</sub> = 8.77	251	1.72
<i>o</i> -Fluoroaniline, C <sub>6</sub> H <sub>6</sub> FN	pK <sub>b</sub> = 10.8	230	9.06
Diphenylamine, C <sub>12</sub> H <sub>11</sub> N	pK <sub>b</sub> = 13.2	282	16.1

Benzoic acid was preliminary purified via the double recrystallization whereas *o*-nitrophenol (Acros organics 99%), piperidine (analytical grade), pyridine (analytical grade), *o*-fluoroaniline (Acros organics 99+%) and diphenylamine (high-purity grade) were used as supplied.

Further,  $2 \times 10^{-3}$  M solutions of these substances in heptane were prepared. 3 mg portions of catalyst samples under study were placed into the flasks with ground stoppers, and 5 ml solution of probe species were added. By measuring absorbance of the solutions before and after their contact with TiO<sub>2</sub> one can estimate the quantity of probe molecules adsorbed and consequently the number of appropriate surface sites according to the formula

$$\nu_{\text{ads}} = \frac{D_0 - D}{\varepsilon \cdot l \cdot m} \cdot V, \quad (1)$$

where  $D_0$  and  $D$  are the absorbance of the solutions before and after their contact with TiO<sub>2</sub> (dimensionless),  $V$  is the solution volume (L),  $l$  is the cell path length (cm),  $\varepsilon$  is the absorption coefficient (L/(cm mol)),  $m$  is the catalyst mass (g).

A low temperature CO adsorption was studied for the TiO<sub>2</sub> and TiO<sub>2</sub>-S samples which were pressed into the tablets with 10–15 mg/cm<sup>2</sup> density. Prior to the CO adsorption, the tablets were treated in vacuum at 150 °C for 90 min. The Bruker Vector 22 FT-IR spectrometer with 2 cm<sup>-1</sup> resolution and 32 scans accumulation regime was used for spectra recording.

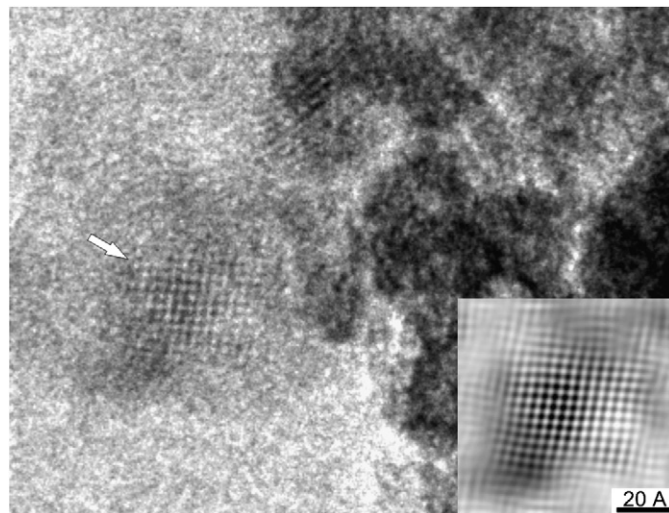
### 2.3. Acetone photocatalytic oxidation

Kinetic measurements were conducted in the flow-circulating system described in detail elsewhere [30,31]. This system includes a quartz reactor thermostated at 40 °C, a membrane circulation pump and a gas module connected with a stainless steel pipes.

Photocatalyst samples were uniformly deposited onto the 3 × 3 cm glass support from aqueous suspension with subsequent drying at room temperature. The density of obtained samples (3 mg/cm<sup>2</sup>) guaranteed the complete absorption of incident light from a 1000 W high-pressure Xe lamp. The lamp irradiation was preliminary transmitted through water and 313-nm interference filters. The UV irradiance was 7 mW/cm<sup>2</sup>.

Input gas mixture consisted from air, water vapor (4500 ± 500 ppm) and acetone vapor (varying from 0 to 6000 ppm). The input and output (after flow-circulating system) gas mixtures were analyzed for the water, acetone and CO<sub>2</sub> content with gas chromatographs equipped with FID and TCD detectors.

The rate of acetone oxidation  $W_{\text{ox}}$  (mol/s) was calculated from the difference between CO<sub>2</sub> concentrations in the output and input



**Fig. 1.** TEM image of TiO<sub>2</sub> Hombifine N.

gas mixtures after the steady state was reached according to the following formula:

$$W_{\text{ox}} = \frac{\Delta C \cdot u \cdot 10^{-9}}{3 \cdot R \cdot T}, \quad (2)$$

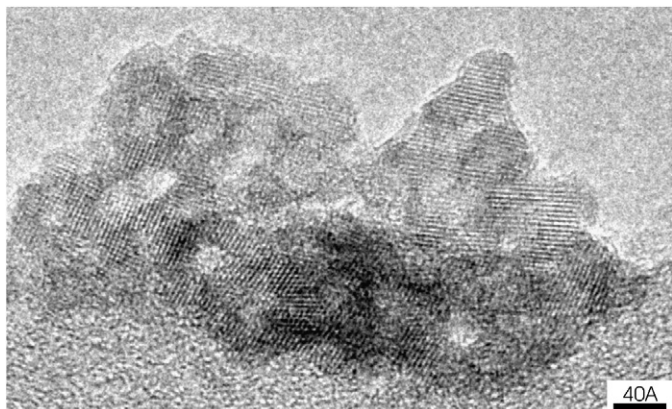
where  $\Delta C$  (ppm) =  $C_{\text{out}} - C_{\text{in}}$  is the difference between CO<sub>2</sub> concentrations in the output and input gas;  $u$  (cm<sup>3</sup>/s) is the gas flow through the flow-circulating system;  $R = 0.082$  (L atm)/(mol K);  $T$  (K) is the temperature. In the present work  $u = 0.58$ – $0.6$  cm<sup>3</sup>/s,  $T = 313$  K,  $\Delta C$  varied from 0 to 500 ppm. Formula (2) uses the fact that one acetone molecule transforms into the three CO<sub>2</sub> molecules during the photocatalytic oxidation and it was controlled at each steady state point by mass balance calculations. It means that no other carbon-containing species except the acetone and CO<sub>2</sub> were detected during the experiments and the ratio  $\Delta C_{\text{CO}_2}/\Delta C_{\text{ac}}$  was practically equal to 3, where  $\Delta C_{\text{CO}_2}$  and  $\Delta C_{\text{ac}}$  are the differences of the inlet and outlet concentrations of CO<sub>2</sub> and acetone correspondingly. The preference of using the  $\Delta C_{\text{CO}_2}$  instead of the directly measuring  $\Delta C_{\text{ac}}$  value in the formula (2) is explained by the fact that at a high acetone concentration the values of  $\Delta C_{\text{ac}}$  become small compared with the absolute inlet acetone concentration. At the same time, the inlet CO<sub>2</sub> concentrations in our experiments was equal to 0 so the  $\Delta C_{\text{CO}_2}$  was equal to outlet CO<sub>2</sub> concentration. In this way, the precision of the  $\Delta C_{\text{CO}_2}$  value was noticeably better than for  $\Delta C_{\text{ac}}$ .

## 3. Results and discussion

### 3.1. Surface investigation

High resolution TEM images of unmodified TiO<sub>2</sub>, modified with sulphuric acid (TiO<sub>2</sub>-S) and with Pt and H<sub>2</sub>SO<sub>4</sub> (TiO<sub>2</sub>-Pt-S) are presented in Figs. 1–3, respectively. All samples are relatively transparent. Therefore images contrast was enhanced for the better view.

The initial TiO<sub>2</sub> consists of primary particles with the size of  $\approx 5$  nm, which are agglomerated into secondary particles of 500–1000 nm diameter. The surface of particles is not clearly defined. The arrow in Fig. 1 shows a single anatase particle with the well defined lattice. The same particle is shown in the lower right part of Fig. 1 after the Fourier filtration. The observed interfacial distance in the lattice is equal to 3.6 Å and the rows are situated at the right angle to each other. The distance coincides well with the lattice constant of anatase  $a = b = 3.733$  Å. Therefore, the observed particle face is believed to correspond to the (001) surface of anatase [32].



**Fig. 2.** TEM image of TiO<sub>2</sub>-S sample. A thin amorphous layer of about 3 Å thickness covers the catalyst surface.

After sulfation under mild conditions, the TiO<sub>2</sub> particles surface underwent significant changes. Surface of the particles is more clearly defined. The main difference in the TiO<sub>2</sub>-S sample shown in Fig. 2 is that one can observe a thin amorphous layer of about 3 Å thickness covering the sample surface. A similar layer was also observed over the surface of sulfated platinumized sample TiO<sub>2</sub>-Pt-S (Fig. 3A). This layer was completely absent in the unmodified initial TiO<sub>2</sub> (Fig. 1). The Pt particle in TiO<sub>2</sub>-Pt-S catalyst is shown in Fig. 3B.

Although the noticeable dissolution of TiO<sub>2</sub> on macroscopic scale occurs only in hot concentrated sulfuric acid [33], interaction with 4 M H<sub>2</sub>SO<sub>4</sub> can result in slight surface dissolution. Mogyorosi with co-workers [34] obtained titanium dioxide samples that contained 72.4 wt% anatase and 27.6 wt% amorphous phase by the sol-gel method in an acidic environment. In [35] the authors reported that amorphous oxo phase of titanium oxide exhibits considerable activity toward photocatalytic degradation of trichloroethylene in the gas phase.

If one calculates the surface sulfur concentration from the data presented in Table 1 it will be equal to about 0.8 atom/nm<sup>2</sup>, i.e. approximately one sulfur atom or SO<sub>4</sub><sup>2-</sup> group per one surface Ti atom. Therefore a thin amorphous layer in our case could be the surface sulfates or the thin TiO(SO<sub>4</sub>) film.

The diameter of Pt particles over the TiO<sub>2</sub>-Pt-S surface was in the range of 1.5–2 nm (Fig. 3B). The calculation of sample surface area occupied by Pt particles based on the total Pt content given in Table 1 provides the value of approximately 0.33–0.44 m<sup>2</sup> per g of the sample. Only a very small portion of the total TiO<sub>2</sub> surface is covered with platinum particles. This agrees well with previous characterizations of Pt-containing TiO<sub>2</sub> of analogous Pt content [27].

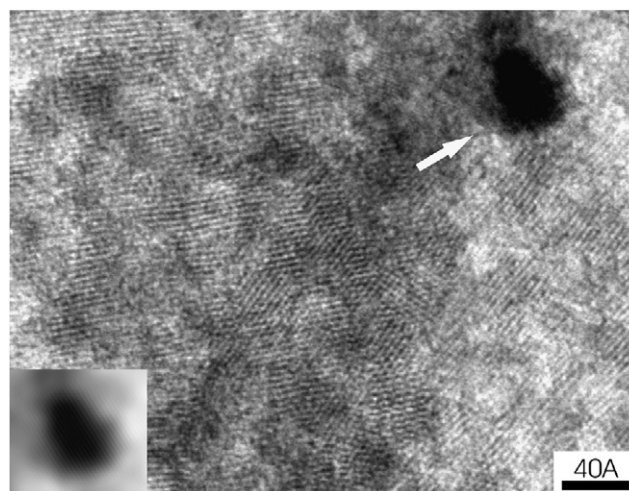
### 3.2. CO adsorption and surface titration

IR spectra of TiO<sub>2</sub> and TiO<sub>2</sub>-S samples treated in vacuum at 150 °C before CO adsorption are shown in Fig. 4. 1235 and 1333 cm<sup>-1</sup> absorption bands appeared after the surface sulfation (spectrum b). The 1333 cm<sup>-1</sup> band is close to the stretching frequency of S=O and the 1200–1250 cm<sup>-1</sup> band is close to the characteristic frequencies of SO<sub>4</sub><sup>2-</sup> [10] with a lower symmetry C<sub>3v</sub> or C<sub>2v</sub> corresponding to mono- and bidentate sulfates [36].

The adsorption of aliquots of CO gives rise to absorption band situated at about 2190 cm<sup>-1</sup> and appearance of absorption band at 2160 cm<sup>-1</sup> at high CO pressure (40 Torr) (Fig. 5). The first type of absorption band corresponds to CO adsorbed on the surface Ti<sup>4+</sup> centers of TiO<sub>2</sub> [37,38]. This band has a gradual shift of its maximum to the lower frequencies (wavenumbers) with the growth



(A)



(B)

**Fig. 3.** TEM images of sample TiO<sub>2</sub>-Pt-S. (A) A thin amorphous layer of about 3 Å thickness can be observed on the surface; (B) the arrow shows the Pt particle. The same particle is shown in the bottom left part of the image after the Fourier filtration. The observed interfacial distance in the metal lattice is equal to 2.3 Å.

of the amount of adsorbed CO. The position of this band is supposed to be the indicator of the strength of surface acidic sites. The stronger shift of this band to the higher wavenumbers relatively to the valence absorption band of gaseous CO (2143 cm<sup>-1</sup> [36]) corresponds to the stronger CO interaction with the surface centers and, therefore, such centers are stronger Lewis acids. Moreover, using the absorption band areas one can estimate the relative or absolute concentrations of surface Lewis sites according to the modified law of absorbance in the form

$$A = A_0 \cdot d \cdot C, \quad (3)$$

where  $A$  is the absorption band area (cm<sup>-1</sup>),  $A_0$  is the CO absorbance coefficient for the particular adsorbent and wavenumber

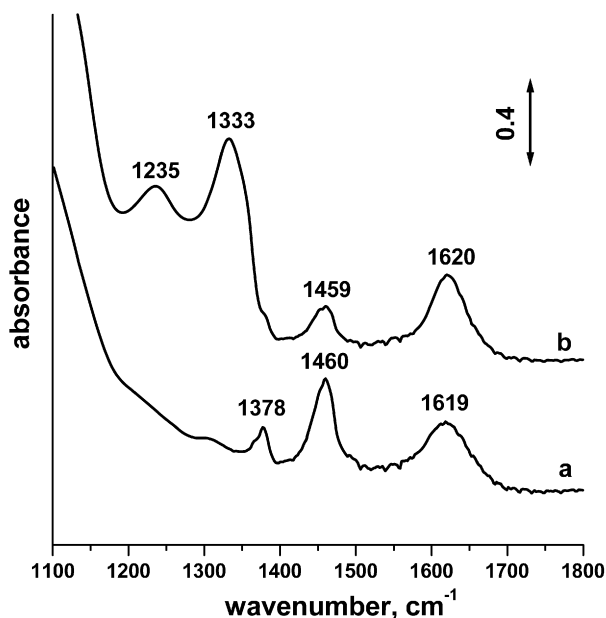


Fig. 4. FTIR spectra of TiO<sub>2</sub> (a) and TiO<sub>2</sub>-S (b) samples treated in vacuum at 150 °C for 90 min. Tablet densities were 15.3 and 11.3 mg/cm<sup>2</sup> for TiO<sub>2</sub> and TiO<sub>2</sub>-S samples, respectively.

(cm/μmol),  $d$  is the tablet density (mg/cm<sup>2</sup>) and  $C$  is the surface sites concentration (mmol/g) [17].

In this way, the surface sites of TiO<sub>2</sub>-S sample are more acidic than those of unmodified TiO<sub>2</sub> since their value of  $\Delta\nu(\text{CO})$  shift to the higher frequency is 3 to 5 cm<sup>-1</sup> higher for TiO<sub>2</sub>-S sample than for pure unmodified TiO<sub>2</sub> (Fig. 5). The difference of CO heats of adsorption for these two samples could be estimated from the following correlation reported by Zaki [39]:

$$\Delta H_{\text{ads}}(\text{CO}) = 10.5 + 0.5 \cdot \Delta\nu(\text{CO}) \text{ kJ mol}^{-1}. \quad (4)$$

The difference  $\Delta H_{\text{ads}}(\text{CO})$  for TiO<sub>2</sub> and TiO<sub>2</sub>-S samples is in the range of 1.5–2.5 kJ mol<sup>-1</sup> indicating that sites strength difference is noticeable but not high.

The ratio of Ti<sup>4+</sup> Lewis sites quantity over sulfated and unsulfated samples derived from the absorbance law varies from 1.4 to 1.6 for the first–third spectra (Figs. 5A and 5B) indicating that the concentration of Lewis sites on the surface of TiO<sub>2</sub>-S sample is about 1.5 times higher.

2157 and 2160 cm<sup>-1</sup> adsorption bands (Fig. 5) correspond to physically adsorbed or H-bonded CO [39] since the corresponding surface OH group valence bands in the 3670–3730 cm<sup>-1</sup> region are decreased and shifted to the lower wavenumbers of 3500–3600 cm<sup>-1</sup> (Figs. 6A and 6B) during the CO adsorption. The total change of IR spectra of TiO<sub>2</sub> and TiO<sub>2</sub>-S samples during the CO adsorption was barely visible. Therefore the resulting IR spectra change in Fig. 6 is represented in the differential form with the subtracted IR spectrum of TiO<sub>2</sub> and TiO<sub>2</sub>-S samples taken before CO adsorption.

In this case one could see that at least 3 types of OH-group vibrations disappear upon CO adsorption on the unmodified TiO<sub>2</sub> sample (Fig. 6A)—3670, 3690 and 3714 cm<sup>-1</sup> adsorption bands; only 2 types of OH-groups vibration bands (Fig. 6B)—3674 and 3713 cm<sup>-1</sup>—decrease upon CO adsorption on the surface of TiO<sub>2</sub>-S sample. It means that, probably, two types of surface OH-groups of pure TiO<sub>2</sub> corresponding to 3670 and 3690 cm<sup>-1</sup> bands were converted into a one type surface OH-groups for the TiO<sub>2</sub>-S sample corresponding to 3674 cm<sup>-1</sup> band during the sample sulfation. In other words, it is possible that there is adsorption of SO<sub>4</sub><sup>2-</sup> ions in the mono- or bidentate forms by the interaction with terminal and

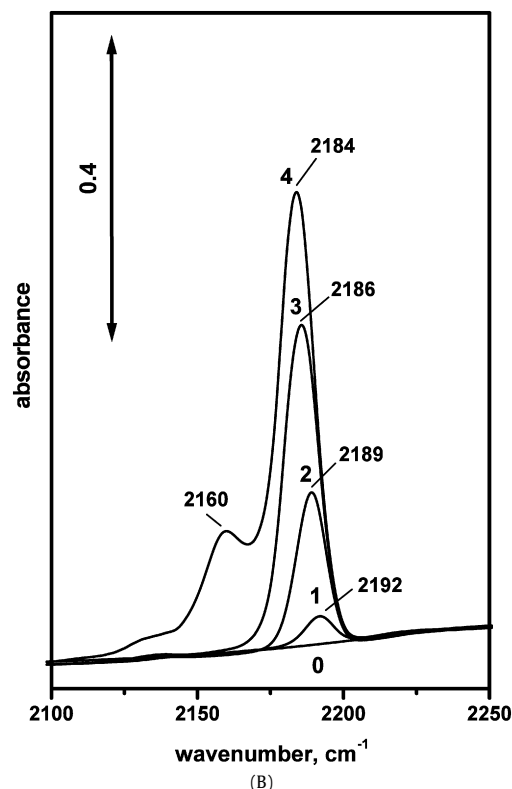
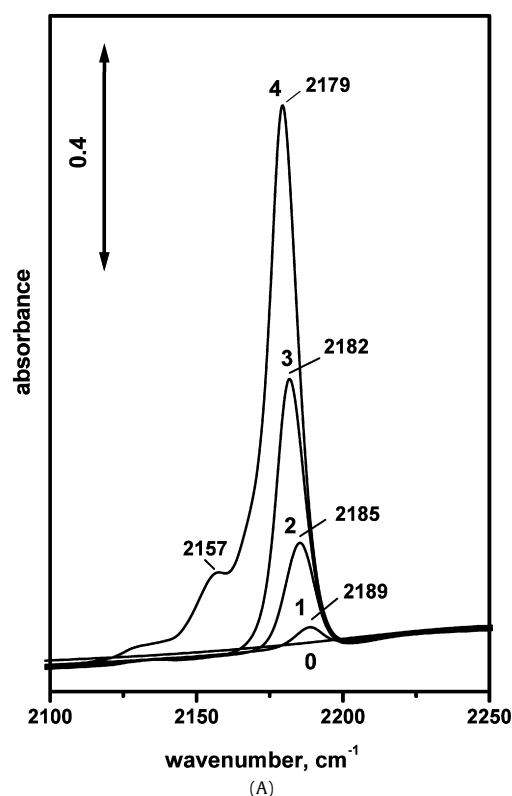
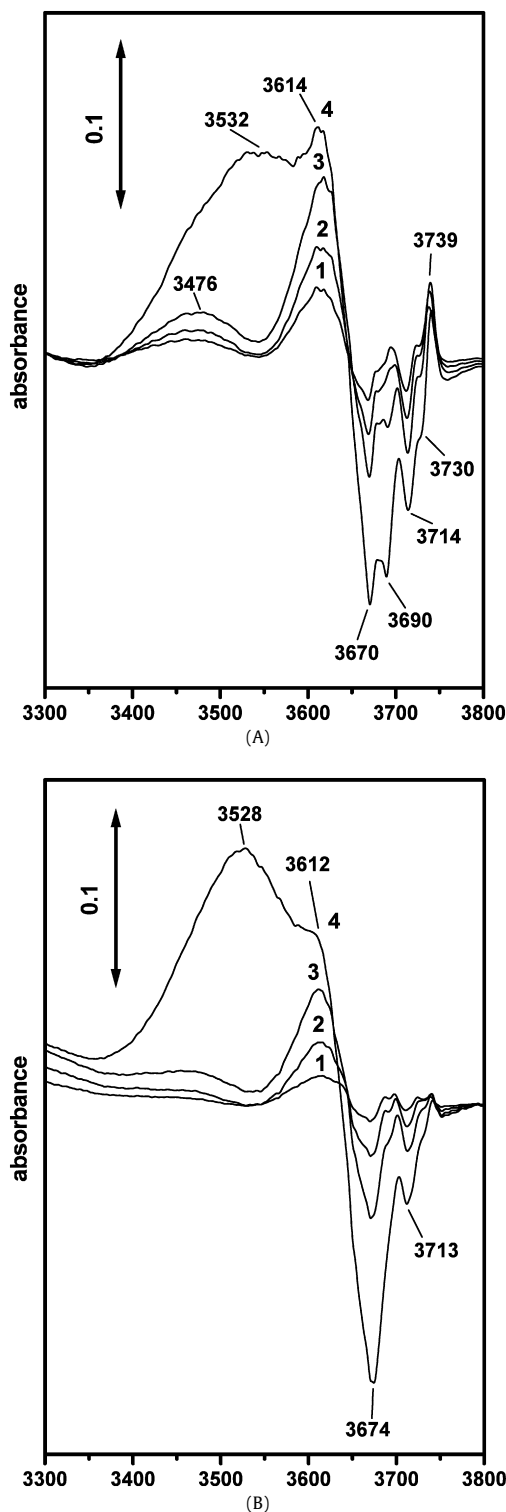


Fig. 5. IR spectra of catalysts during low temperature CO adsorption: (A) TiO<sub>2</sub>, (B) TiO<sub>2</sub>-S. Numerals above the spectra correspond to CO pressure: (0) no CO admission; (1) 3 Torr; (2) 11 Torr; (3) 21 Torr; (4) 40 Torr. Tablet densities were 15.3 and 11.3 mg/cm<sup>2</sup> for the TiO<sub>2</sub> and TiO<sub>2</sub>-S samples, respectively.

bridge OH-groups that converts them into the one type of S atom bonded OH-groups.

Another very powerful method to study acid–base surface sites is adsorption of probe molecules from solutes [40,41]. Results of



**Fig. 6.** Changes of IR spectra of  $\text{TiO}_2$  (A) and  $\text{TiO}_2\text{-S}$  (B) in the valence OH vibrations region during the CO adsorption. All the spectra are the result of subtraction of the initial spectrum of the samples before CO adsorption.

the  $\text{TiO}_2$ ,  $\text{TiO}_2\text{-S}$  and  $\text{TiO}_2\text{-Pt-S}$  samples titration by probe organic species are presented in Table 3. In our previous research [17] only one type of organic base and acid was used for titration giving the correlation of activity with the total quantity of surface acidic and basic sites. An attempt to classify the range of acidic sites by their strength is done in the present work.

The strongest species—benzoic acid ( $\text{p}K_a = 4.2$ ) and base piperidine ( $\text{p}K_b = 2.88$ )—should adsorb on a variety of basic and

**Table 3**

Quantity of adsorbed probe species on the surface of  $\text{TiO}_2$ ,  $\text{TiO}_2\text{-S}$  and  $\text{TiO}_2\text{-Pt-S}$  samples

Probe species	Strength, $\text{p}K$	Adsorbed quantity, mmol/g (molecules/ $\text{nm}^2$ )		
		$\text{TiO}_2$	$\text{TiO}_2\text{-S}$	$\text{TiO}_2\text{-Pt-S}$
<b>Acids</b>				
Benzoic acid	$\text{p}K_a = 4.2$	1.25 (2.2)	0.96 (1.7)	0.66 (1.2)
<i>o</i> -Nitrophenol	$\text{p}K_a = 7.17$	0.60 (1.1)	0.27 (0.5)	0.08 (0.1)
<b>Bases</b>				
Piperidine	$\text{p}K_b = 2.88$	0.85 (1.5)	1.13 (2)	0.77 (1.4)
Pyridine	$\text{p}K_b = 8.77$	0.67 (1.2)	0.72 (1.3)	0.47 (0.8)
<i>o</i> -Fluoroaniline	$\text{p}K_b = 10.8$	0.23 (0.4)	0.50 (0.9)	0.24 (0.4)
Diphenylamine	$\text{p}K_b = 13.2$	0.16 (0.3)	0.28 (0.5)	0.20 (0.35)

acidic sites, respectively, giving the highest quantity of adsorbed probe species for all the three studied samples (Table 3). At the same time, the weakest acid, *o*-nitrophenol ( $\text{p}K_a = 7.17$ ), and base, diphenylamine ( $\text{p}K_b = 13.2$ ), should adsorb only on relatively strong basic and acidic sites giving the lowest quantity of adsorbed species. In this assumption we have neglected the possible specific adsorption of some of the probe species which was not investigated in this work. One should keep in mind that specific adsorption can result in an over-estimation of surface sites quantity compared with the actual one.

Colon with co-workers [9] estimated the total quantity of acid sites on the surface of sulfated  $\text{TiO}_2$  to be equal to  $1 \mu\text{mol}/\text{m}^2$  by the microcalorimetric pyridine adsorption. The highest concentration for  $\text{TiO}_2\text{-S}$  sample (Table 3) is equal to  $1.13 \text{ mmol}/\text{g}$  or  $3.3 \mu\text{mol}/\text{m}^2$  although the  $\text{SO}_4^{2-}$  species surface concentration is even higher in our case. Thus, the mild sulfation technique produces higher surface concentration of acidic groups.

The comparison of adsorption data for pure  $\text{TiO}_2$  and  $\text{TiO}_2\text{-S}$  samples (Table 3) shows that quantity of basic sites (total and only strong) decrease after the  $\text{H}_2\text{SO}_4$  treatment. At the same time, quantities of acidic sites are increased including the most strong ones measured by diphenylamine titration. The ratio of acid sites quantities for  $\text{TiO}_2\text{-S}$  and  $\text{TiO}_2$  samples is equal to 1.33, 1.07, 2.17 and 1.75 for piperidine, pyridine, *o*-fluoroaniline and diphenylamine, respectively, and is in satisfactory agreement with the CO absorption band intensities ratio which is equal to about 1.5. Therefore, both methods give the correlating results about quantity and strength of acidic centers.

The quantity of strong acidic sites on the surface of platinumized  $\text{TiO}_2\text{-Pt-S}$  sample is equal to  $0.2 \text{ mmol}/\text{g}$  and is also greater than for pure  $\text{TiO}_2$  sample. At the same time, the total acidity measured by piperidine adsorption is the lowest among the three studied samples (Table 3). The quantity of basic sites over  $\text{TiO}_2\text{-Pt-S}$  sample is two-fold lower than for initial  $\text{TiO}_2$  and about 1.5-fold lower than for sulfated  $\text{TiO}_2$ . Such a decrease in acid and base sites quantity in  $\text{TiO}_2\text{-Pt-S}$  is unexpected and cannot be explained by surface blocking by Pt particles since their surface was estimated above and is equal to just  $0.33\text{--}0.44 \text{ m}^2/\text{g}$ . Moreover, in the next section it will be demonstrated that  $\text{TiO}_2\text{-Pt-S}$  sample possesses the highest photoactivity.

In our previous work [30] it was shown that treatment of  $\text{TiO}_2$  with  $\text{NaBH}_4$  which we are using for Pt reduction even without additions of  $\text{H}_2\text{PtCl}_6$  resulted in significant changes of catalytic properties. Namely, the treated catalyst possessed lower activity in the low temperature range but higher activity at elevated temperatures and higher stability toward thermal deactivation in acetone photocatalytic oxidation. Adsorbed boron species probably in the form of borates can effectively block the  $\text{Ti}^{4+}$  surface species that are responsible for surface acidic sites. That is why in the kinetic experiments we additionally investigated  $\text{TiO}_2$  with 1% of deposited Pt but without further acidic treatment (marked as  $\text{TiO}_2\text{-Pt}$ ) to elucidate the effect of sulfation on the photooxidation rate.

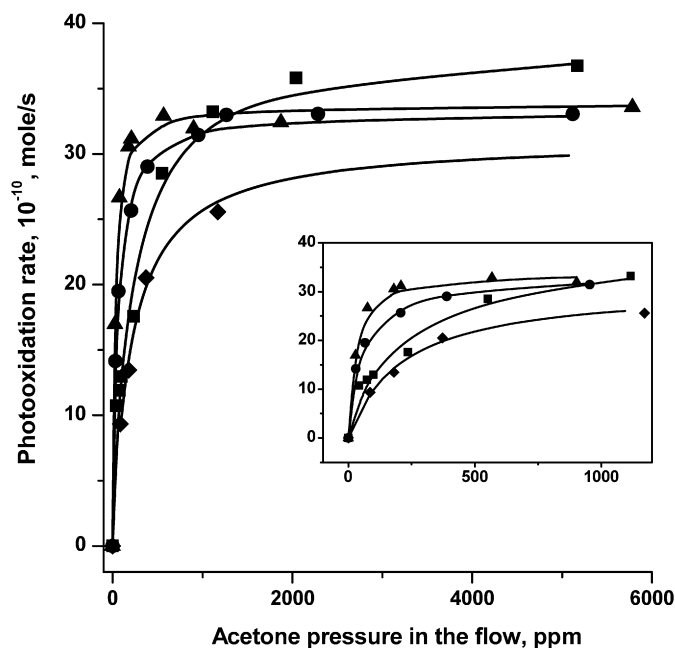


Fig. 7. Steady-state acetone photocatalytic oxidation rate as a function of its concentration in the flow-circulating reactor for different photocatalysts: (■)  $\text{TiO}_2$ ; (●)  $\text{TiO}_2\text{-S}$  and (▲)  $\text{TiO}_2\text{-Pt-S}$ , (◆)  $\text{TiO}_2\text{-Pt}$ . In the inset is shown the region of small concentrations.

### 3.3. Kinetics of acetone vapor photocatalytic oxidation

The dependence of the steady-state rates of the acetone vapor photocatalytic oxidation on its concentration for  $\text{TiO}_2$ ,  $\text{TiO}_2\text{-S}$ ,  $\text{TiO}_2\text{-Pt-S}$  and  $\text{TiO}_2\text{-Pt}$  samples is shown in Fig. 7. All the data points are well described by the one adsorption site Langmuir–Hinshelwood equation:

$$W_{\text{OX}} = \frac{k_r \cdot K_{\text{ads}} \cdot C}{1 + K_{\text{ads}} \cdot C}, \quad (5)$$

where  $k_r$  and  $K_{\text{ads}}$  are the photooxidation rate and acetone adsorption constants;  $C$  is the acetone gas phase concentration. Constant  $k_r$  in this equation also could be considered as the maximum photooxidation rate at high acetone concentration ( $K_{\text{ads}} \cdot C \gg 1$ ). Solid curves shown in Fig. 7 are the result of approximation of experimental data. Calculated values of  $k_r$  and  $K_{\text{ads}}$  are listed in Table 4.

Constant  $k_r$  is equal to  $33 \times 10^{-10}$  mol/s for  $\text{TiO}_2\text{-Pt-S}$  and  $\text{TiO}_2\text{-S}$  samples and is slightly higher ( $38 \times 10^{-10}$  mol/s) and slightly lower ( $31 \times 10^{-10}$  mol/s) for pure  $\text{TiO}_2$  and  $\text{TiO}_2\text{-Pt}$  samples, correspondingly. The curves in Fig. 7 show that at acetone concentration above 1500 ppm, unmodified  $\text{TiO}_2$  possesses the highest oxidation rate that is connected with the highest rate constant for this sample whereas  $\text{TiO}_2\text{-Pt}$  demonstrates the lowest oxidation rate that we believe is associated with partial blocking of  $\text{TiO}_2$  surface with boron species produced from the  $\text{NaBH}_4$  treatment.

In general, at high acetone concentration levels (>1500 ppm) all samples have similar photocatalytic activity because the acetone monolayer formation has been completed on samples surfaces. Under these conditions the value of adsorption constant  $K_{\text{ads}}$  does not play any significant role and activity is determined by the quantity of active sites and turnover rate. The quantity of active sites can be estimated as equal if one takes it proportional to the surface area, which in turn is similar for all samples. Thus, turnover rate is also similar for all the catalysts. This means that the electron–hole separation is also similar for sulfated and untreated samples in contrast to hypothesis of works [12,13].

In many cases contaminants concentrations are low and are not enough for significant surface coverage of photocatalyst. Under

Table 4  
Results of approximation of acetone photocatalytic oxidation by the Langmuir–Hinshelwood model (5)

Sample	$k_r$ , $10^{-10}$ , mol/s	$K_{\text{ads}}$ , $\text{ppm}^{-1}$
1% Pt/ $\text{TiO}_2$ (unsulfated)	$31.13 \pm 0.5$	$4.7 \times 10^{-3} \pm 3.8 \times 10^{-4}$
$\text{TiO}_2$	$38.3 \pm 1.5$	$5.3 \times 10^{-3} \pm 8.3 \times 10^{-4}$
$\text{TiO}_2\text{-S}$	$33.2 \pm 0.4$	$2.2 \times 10^{-2} \pm 1.8 \times 10^{-3}$
$\text{TiO}_2\text{-Pt-S}$	$33.8 \pm 0.5$	$4.1 \times 10^{-2} \pm 4.4 \times 10^{-3}$

such conditions, the adsorption characteristics of the photo(catalyst) have the critical importance. This situation corresponds to the low acetone concentration level (<500 ppm).

The inset in Fig. 7 shows the photocatalytic oxidation rates in this low concentration range. The  $\text{TiO}_2\text{-Pt}$  catalyst is still the least active sample. Pure  $\text{TiO}_2$  sample has a bit higher rate of photooxidation. The sulfated  $\text{TiO}_2\text{-S}$  sample has intermediate activity and the highest activity is demonstrated by the platinumized and sulfated  $\text{TiO}_2\text{-Pt-S}$  sample. For example, at the acetone concentration level near 150 ppm the PCO rate close to 13, 16, 24 and  $29 \times 10^{-10}$  mol/s values for  $\text{TiO}_2\text{-Pt}$ ,  $\text{TiO}_2$ ,  $\text{TiO}_2\text{-S}$  and  $\text{TiO}_2\text{-Pt-S}$  samples, respectively. Moreover, at the lower acetone concentration levels this difference will be even higher indicating that in such low concentration conditions the sulfated and especially sulfated platinumized  $\text{TiO}_2$  samples work more than 3 times effectively.

Here we have to discuss two moments. On the one hand, there is the dramatic increase of adsorption properties of platinumized  $\text{TiO}_2$  treated with sulphuric acid ( $\text{TiO}_2\text{-Pt-S}$ ) against the untreated one. Indeed, the sulfation procedure increased the  $K_{\text{ads}}$  by an order of magnitude from 0.0047 to 0.041  $\text{ppm}^{-1}$ . The absolutely similar sulfation procedure in the case of non-platinumized  $\text{TiO}_2$  resulted in only 4 time increase of  $K_{\text{ads}}$  from 0.0053 to 0.022  $\text{ppm}^{-1}$  value. The stronger influence of sulfation procedure on the photoactivity of Pt-loaded  $\text{TiO}_2$  samples probably could be explained by the removal of oxygen containing boron species from  $\text{TiO}_2$  surface. Such species could form as a result of  $\text{NaBH}_4$  oxidation with  $\text{H}_2\text{PtCl}_6$  during the chemical deposition procedure.

On the other hand, there is not a big difference in adsorption constant between Hombifine  $\text{TiO}_2$  and its platinumized form  $\text{TiO}_2\text{-Pt}$  but more than two-fold increase in adsorption constant for  $\text{TiO}_2\text{-Pt-S}$  as compared to  $\text{TiO}_2\text{-S}$  samples. We attribute this behavior to the suppressing influence of Pt-deposition procedure which produces the oxygen containing boron species on the  $\text{TiO}_2$  surface. In fact, in the case of  $\text{TiO}_2$  and  $\text{TiO}_2\text{-Pt}$  samples, the possible positive effect of Pt deposition was suppressed by the adsorbed boron species unlike the case of  $\text{TiO}_2\text{-S}$  and  $\text{TiO}_2\text{-Pt-S}$  samples where the sulfation procedure after the Pt-deposition washed out the boron species. Two additional observations support this assumption:

- (1) A  $^{11}\text{B}$  NMR signal was observed in the  $\text{TiO}_2\text{-Pt}$  sample corresponding to the 0.012 wt% of tetrahedral  $\text{BO}_4$  species. And this signal was not observed in the  $\text{TiO}_2\text{-Pt-S}$  sample giving us an idea that it was simply washed out during the sulfation procedure.
- (2) The sample prepared by the reverse sequence, i.e. Pt deposition was done after the sulfation procedure ( $\text{TiO}_2\text{-S-Pt}$ ), demonstrated a lower photocatalytic activity than  $\text{TiO}_2\text{-Pt-S}$  sample but still higher than untreated and platinumized  $\text{TiO}_2$  and  $\text{TiO}_2\text{-Pt}$  samples in the flow-circulating system at the 500 ppm acetone vapor pressure. It means that there are remaining boron species on the surface of  $\text{TiO}_2\text{-S-Pt}$  sample suppressing its photoactivity just because the Pt-deposition procedure was the last.

Based upon the data above we could say that in any case the sulfation procedure makes the more pronounced effect on the  $\text{TiO}_2$

photoactivity against VOC's PCO unlike the Pt chemical deposition based on the  $\text{H}_2\text{PtCl}_6$  reduction with  $\text{NaBH}_4$ .

Most probably, an additional study of the surface state before and after the reaction would expand our understanding of the origin of high photocatalytic activity at the low acetone concentration level. In our opinion such investigations should include comparative FTIR reflectance spectroscopy of  $\text{TiO}_2$  surface in the course of prolonged PCO experiments to accumulate the surface changes.

#### 4. Conclusions

Low temperature CO adsorption and titration with dissolved organic probe species were used for characterization of surface acid and base sites of pure and sulfated  $\text{TiO}_2$  catalyst. The agreeing results indicate that the quantity and strength of surface acid sites increases as a result of this treatment. Deposition of platinum and sulfation decreases the number of surface acid and base sites compared to sulfated  $\text{TiO}_2$ .

The dependence of steady-state rate of acetone vapor photocatalytic oxidation for  $\text{TiO}_2$ ,  $\text{SO}_4^{2-}/\text{TiO}_2$ , (1% Pt)/ $\text{TiO}_2$  and (1% Pt,  $\text{SO}_4^{2-}$ )/ $\text{TiO}_2$  samples obeys the Langmuir–Hinshelwood kinetic model. All samples have a similar activity in the high acetone concentration range that signifies the completion of acetone monolayer coverage on the surface.

In the low concentration range, the more acidic sulfated  $\text{TiO}_2$  possesses a higher photocatalytic activity due to the increase of acetone adsorption constant which correlates with the surface acidity according to CO and organic probe species adsorption data.

The highest photoactivity of (1% Pt,  $\text{SO}_4^{2-}$ )/ $\text{TiO}_2$  sample can be explained by cumulative effect of platinum and  $\text{SO}_4^{2-}$  addition on acetone adsorption constant.

#### Acknowledgments

Support by NATO Sfp-981461 and ISTC 3305 grants is gratefully acknowledged. One of the authors (D.V.K.) appreciates the support of the "Russian Science Support Foundation."

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